

# Microcombustor modeling using the RBF-FD method

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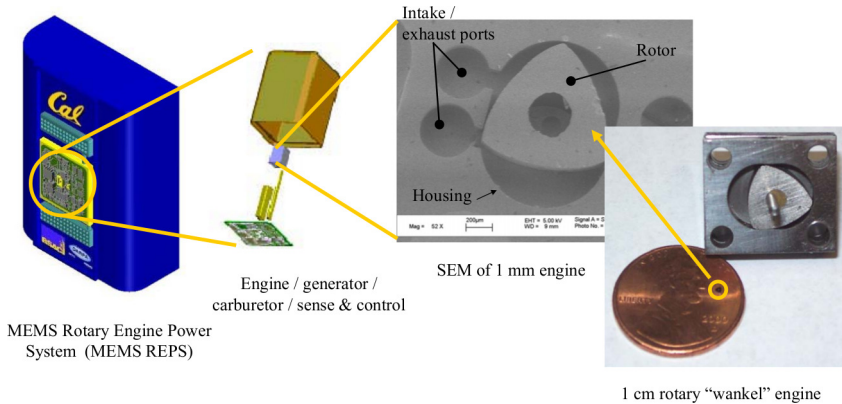
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- 1 Introduction
- 2 Mathematical model
- 3 Numerical implementation
- 4 Validation and convergence
- 5 Numerical experiments
- 6 Conclusions

- 1 Introduction
- 2 Mathematical model
- 3 Numerical implementation
- 4 Validation and convergence
- 5 Numerical experiments
- 6 Conclusions

# Micro rotary engine



**Figure :** Sketch of a micro-rotary engine from the *Micro-Rotary Combustion Lab, University of California, Berkeley.*

## Microscale combustion

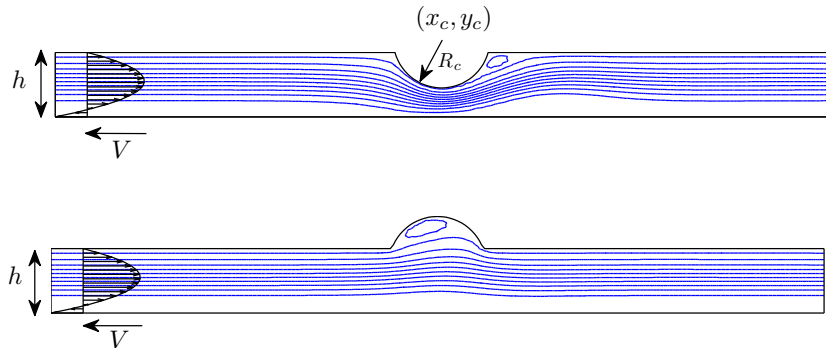
- nano and micro technology devices require *compact* and *rechargeable* power supplies
- at present these devices rely on *batteries*
- but *energy density* of batteries is very low:
  - 0.7 MJ/kg for lithium-ion batteries
  - several hours to recharge
- possible alternative: *micro-engines*
  - hydrocarbon fuels have 45 MJ/Kg of stored chemical energy
  - an efficiency of 5% in converting this energy to electricity will outperform batteries
- small-scale *rotary engine* (Fernández-Pello, 2002)
  - high specific power
  - low cost due to: minimum number of moving parts and no valves required for operation
  - mechanical shaft output can be directly coupled to electric motor

- 1 Introduction
- 2 Mathematical model**
- 3 Numerical implementation
- 4 Validation and convergence
- 5 Numerical experiments
- 6 Conclusions

# Model

- Combustion chamber is approximated by a 2D channel.
- Bottom wall moves with velocity  $\pm V$  relative to the other.
- Upper wall has a notch which modifies the combustible flow and facilitates the attachment of the flame.
- The velocity profile at the inlet is the sum of a Poiseuille flow and a Couette flow.
- When the mixture flows through the channel, a recirculation zone appears due to the notch.
- If the mixture is ignited, a steady flame might be established in the channel.
- Its structure and location depends on the flow rate which determines the attachment position, among other parameters.

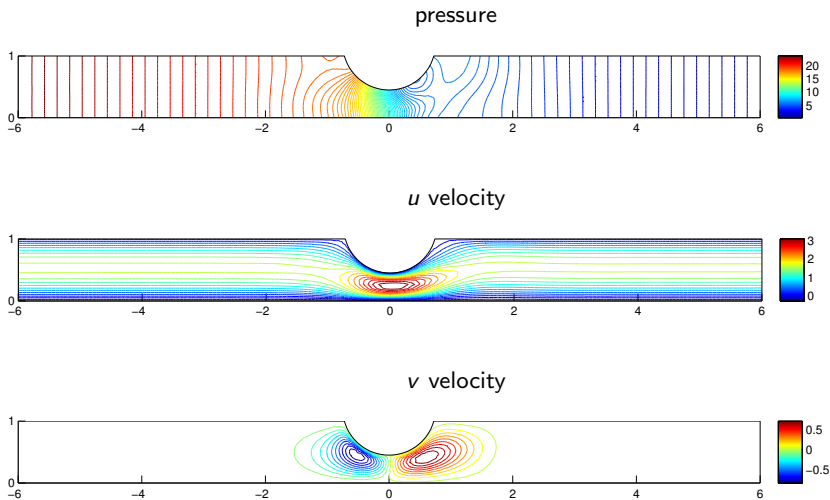
# Micro rotary engine: flow results



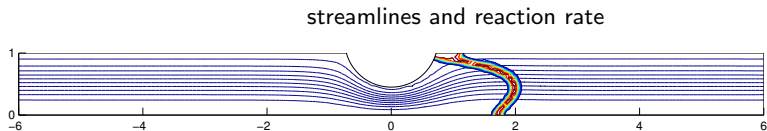
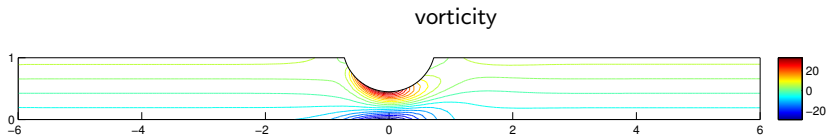
**Figure :** Channel configurations for an inner notch (up) and an outer notch (down). The flow field is illustrated by selected streamlines.



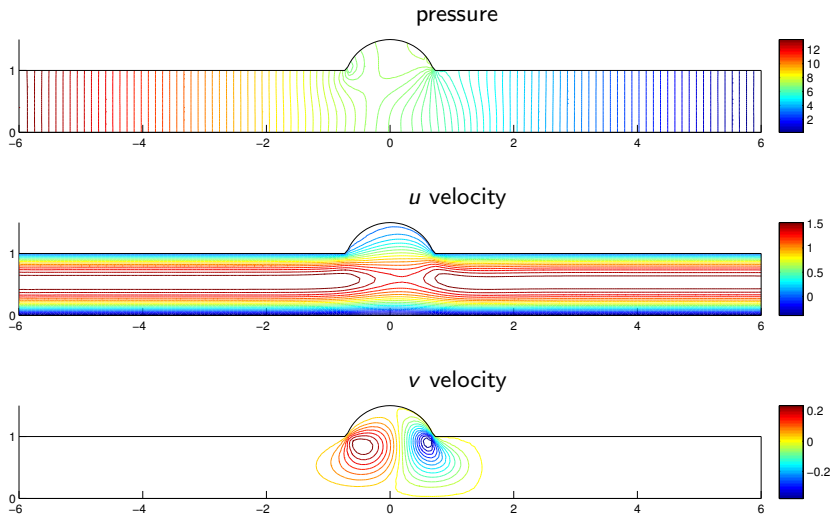
$m = 2$ , wall velocity  $V = -0.5$ .



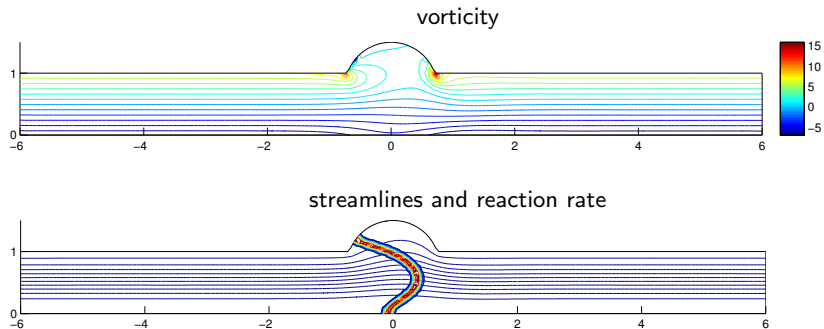
$m = 2$ , wall velocity  $V = -0.5$ .



$m = 2$ , wall velocity  $V = -0.5$ .



$m = 2$ , wall velocity  $V = -0.5$ .



## Parameters

|                 |                                   |
|-----------------|-----------------------------------|
| $m$             | mass flow                         |
| $Pr = 0.7$      | Prandlt number                    |
| $Pe$            | Peclet number                     |
| $Re = Pe/Pr$    | Reynolds number                   |
| $Ze = 10$       | Zeldovich number                  |
| $u_p = u_p(Le)$ | $S_L/U_L$                         |
| $\gamma = 0.7$  | heat release parameter            |
| $V$             | wall velocity                     |
| $\kappa$        | heat loss coefficient             |
| $\theta_m$      | temperature in combustion chamber |

## Thermo-diffusive model of flame propagation

The flow is assumed to be independent of the combustion, and is described by the continuity and momentum equations

$$\begin{cases} \nabla \cdot \mathbf{u} & = 0 \\ (\mathbf{u} \cdot \nabla) \mathbf{u} & = -\nabla p + \frac{1}{\text{PePr}} \nabla^2 \mathbf{u} \end{cases} \quad (1)$$

The propagation of premixed flames subject to the previous flow is described by

$$\begin{cases} \frac{\partial \theta}{\partial t} + \text{Pe} (\mathbf{u} \cdot \nabla) \theta & = \nabla^2 \theta + \text{Pe}^2 \omega(\theta, Y) \\ \frac{\partial Y}{\partial t} + \text{Pe} (\mathbf{u} \cdot \nabla) Y & = \frac{1}{\text{Le}} \nabla^2 Y - \text{Pe}^2 \omega(\theta, Y) \end{cases} \quad (2)$$

where  $\theta$  is the temperature,  $Y$  is the fuel mass fraction and  $\omega(\theta, Y)$  is the reaction rate,

$$\omega(\theta, Y) = \frac{\text{Ze}^2}{2 \text{Le} u_p^2} Y \exp \left[ \frac{\text{Ze}(\theta - 1)}{1 + \gamma(\theta - 1)} \right]. \quad (3)$$

## Boundary conditions

$$y = 0 : \quad u = V, \quad v = 0, \quad \frac{\partial \theta}{\partial \vec{n}} = \kappa Pe (\theta - \theta_m), \quad \frac{\partial Y}{\partial \vec{n}} = 0,$$

$$y = y_s(x) : \quad u = v = 0, \quad \frac{\partial \theta}{\partial \vec{n}} = 0, \quad \frac{\partial Y}{\partial \vec{n}} = 0.$$

$$x \rightarrow -\infty, \quad \begin{cases} u(y) = -6my^2 + (6m - V)y + V, & v = 0 \\ Y = 1, & \theta = \theta_m \end{cases}$$

$$x \rightarrow +\infty, \quad \frac{\partial u}{\partial x} = \frac{\partial v}{\partial x} = 0, \quad \frac{\partial Y}{\partial x} = \frac{\partial \theta}{\partial x} = 0.$$

## Domain and initial conditions

Channel length:  $[L_0, L_f]$ . Width = 1. Upper boundary:

$$y_s(x) = 1 + ae^{-bx^2}, \quad (4)$$

where  $a$  and  $b$  control the depth and width of the notch.

Initial conditions:

- Hot spot:

$$\begin{aligned} \theta(0) &= \theta_{ig} e^{-r^2/\delta^2}, & r^2 &= (x - x_{ig})^2 + (y - y_{ig})^2 \\ Y(0) &= 1 \end{aligned} \quad (5)$$

where  $x_{ig}$ ,  $y_{ig}$ ,  $\theta_{ig}$  and  $\delta$  are parameters that define the location, intensity and decay rate of the initial hot spot

- Planar flame speed in channel (for  $a = 0$ ):

$$\begin{aligned} Y(0) &= 1 / \left( 1 + e^{c(x+1)} \right) \\ \theta(0) &= \theta_m + (1 - \theta_m)(1 - Y(x)) \end{aligned} \quad (6)$$



- 1 Introduction
- 2 Mathematical model
- 3 Numerical implementation**
- 4 Validation and convergence
- 5 Numerical experiments
- 6 Conclusions

## Navier-Stokes equations

Stream function formulation,

$$u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x};$$

the Navier-Stokes equations take the form

$$\Delta^2 \psi + PePr \left[ \frac{\partial \psi}{\partial x} \frac{\partial \Delta \psi}{\partial y} - \frac{\partial \psi}{\partial y} \frac{\partial \Delta \psi}{\partial x} \right] = 0 \quad (7)$$

with boundary conditions

$$y = 0 : \quad \psi = 0, \quad \frac{\partial \psi}{\partial \vec{n}} = V.$$

$$y = y_s(x) : \quad \psi = m + V/2, \quad \frac{\partial \psi}{\partial \vec{n}} = 0.$$

As  $x \rightarrow -\infty$ ,

$$\psi(y) = -2my^3 + (3m - V/2)y^2 + Vy, \quad \frac{\partial \psi}{\partial x} = 0. \quad (8)$$

As  $x \rightarrow +\infty$ ,

$$\frac{\partial^2 \psi}{\partial x \partial y} = 0; \quad \frac{\partial^2 \psi}{\partial x^2} = 0. \quad (9)$$

## Navier-Stokes equations

Equation (7) is solved with Newton's method.

- Initial approximation  $\psi^{(0)}$

- at each iteration compute  $\psi^{(i)} = \psi^{(i-1)} + \xi$ , where the correction  $\xi$  is the solution of

$$\Delta^2 \xi + PePr \left[ \frac{\partial \psi^{(i-1)}}{\partial x} \frac{\partial \Delta \xi}{\partial y} - \frac{\partial \psi^{(i-1)}}{\partial y} \frac{\partial \Delta \xi}{\partial x} + \frac{\partial \xi}{\partial x} \frac{\partial \Delta \psi^{(i-1)}}{\partial y} - \frac{\partial \xi}{\partial y} \frac{\partial \Delta \psi^{(i-1)}}{\partial x} \right] = R(\psi^{(i-1)}) \quad (10)$$

- with boundary conditions

$$B\xi = g(x, y) - B\psi^{(i-1)}. \quad (11)$$

- $R(\psi^{(i-1)})$  is the residual at iteration  $i$

$$R(\psi^{(i-1)}) = \Delta^2 \psi^{(i-1)} + PePr \left[ \frac{\partial \psi^{(i-1)}}{\partial x} \frac{\partial \Delta \psi^{(i-1)}}{\partial y} - \frac{\partial \psi^{(i-1)}}{\partial y} \frac{\partial \Delta \psi^{(i-1)}}{\partial x} \right], \quad (12)$$

- iterations continue until  $\|R(\psi^{(i-1)})\| \leq \epsilon$
- RBF-FD with polynomial augmentation is used to discretize differential operators.
- at each iteration equations (10) are solved using a direct solver.

# Combustion equations

$$\begin{aligned}
 \frac{\partial \theta}{\partial t} &= \left[ \nabla^2 - \text{Pe} (\mathbf{u} \cdot \nabla) \right] \theta + \text{Pe}^2 \cdot \omega(\theta, Y) \\
 \frac{\partial Y}{\partial t} &= \left[ \frac{1}{Le} \nabla^2 - \text{Pe} (\mathbf{u} \cdot \nabla) \right] Y - \text{Pe}^2 \cdot \omega(\theta, Y)
 \end{aligned}
 \tag{13}$$

- Spatial differential operators: are discretized (in a preprocessing step) using RBF-FD augmented with polynomials.  $\Rightarrow$  sparse differential matrices

$$\begin{aligned}
 D_{\theta} &= \nabla^2 - \text{Pe} (\mathbf{u} \cdot \nabla), \\
 D_Y &= \frac{1}{Le} \nabla^2 - \text{Pe} (\mathbf{u} \cdot \nabla).
 \end{aligned}$$

## Combustion equations

- Time integration: semi-implicit CN-AB2 (implicit for the linear terms and explicit for the non-linear terms).

$$\begin{aligned} \left( \mathbb{I} - \frac{\Delta t}{2} D_{\theta} \right) \theta^{k+1} &= \left( \mathbb{I} + \frac{\Delta t}{2} D_{\theta} \right) \theta^k + \frac{\Delta t}{2} \cdot \left( 3G^k - G^{k-1} \right) \\ \left( \mathbb{I} - \frac{\Delta t}{2} D_Y \right) Y^{k+1} &= \left( \mathbb{I} + \frac{\Delta t}{2} D_Y \right) Y^k - \frac{\Delta t}{2} \cdot \left( 3G^k - G^{k-1} \right) \end{aligned} \quad (14)$$

- (14) together with boundary conditions, are solved at each time step using iterative solver BiCGSTAB with iLU as preconditioner.  $G^k$  represents the non-linear term

$$G^k = \text{Pe}^2 \cdot \omega(\theta^k, Y^k).$$

- Iterations continue until  $\|\theta^k - \theta^{k-1}\| \leq \text{tol}$  and  $\|Y^k - Y^{k-1}\| \leq \text{tol}$  (tol =  $10^{-8}$ ).

## Domain discretization:

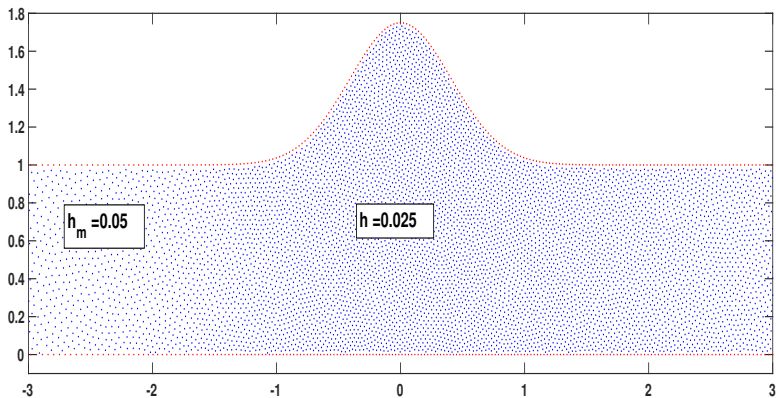
The domain is discretized using scattered nodes with an inter-nodal distance  $\Delta$  controlled by a predefined function

$$\Delta = h + (h_m - h) [1/(1 + \exp(2(x + 3))) + 1/(1 + \exp(-(x - 3)))], \quad (15)$$

where  $h_m$  and  $h$  are the inter-nodal distances away and near the notch, respectively. Ideally, a fine node distribution is used near the notch, becoming coarser towards the extremes of the channel.

A layer of ghost nodes is introduced all around the domain, so that:

- 1 the eight boundary conditions from the biharmonic equation (NS equations in the streamline formulation) can be satisfied.
- 2 The Runge phenomenon is avoided near boundaries.



The spatial differential operators are approximated using PHS  $r^7$  with polynomial augmentation up to  $m$ -th degree. The expected convergence is  $O(h^m)$  for the combustion equations and  $O(h^{m-2})$  for the biharmonic equation. V. Bayona, N. Flyer, B. Fornberg. G.A. Barnett, *J. Comput. Phys.* (2017).

- 1 Introduction
- 2 Mathematical model
- 3 Numerical implementation
- 4 Validation and convergence**
- 5 Numerical experiments
- 6 Conclusions

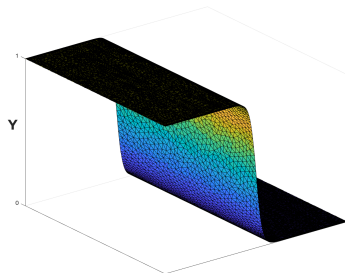
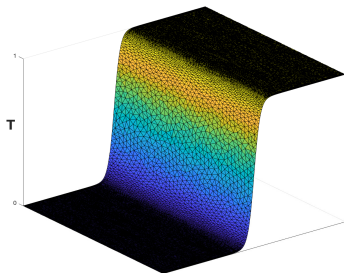


## Planar adiabatic flame



$$\begin{cases} \frac{\partial \theta}{\partial t} + u_p \frac{\partial \theta}{\partial x} = \Delta \theta + \omega \\ \frac{\partial Y}{\partial t} + u_p \frac{\partial Y}{\partial x} = \frac{1}{Le} \Delta Y - \omega \end{cases}$$

$$x \rightarrow -\infty, \quad \theta = Y - 1 = 0, \quad x \rightarrow \infty, \quad \theta - 1 = Y = 0$$



Planar adiabatic flame,  $u_p$  vs  $Le$ 

Fig 2 V. N. Kurdyumov, Combustion and Flame, 158 (2011)

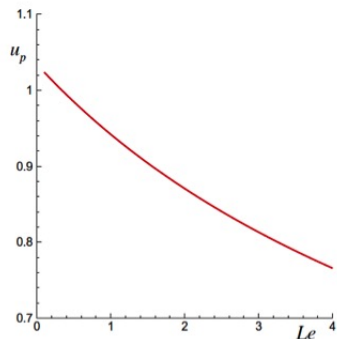
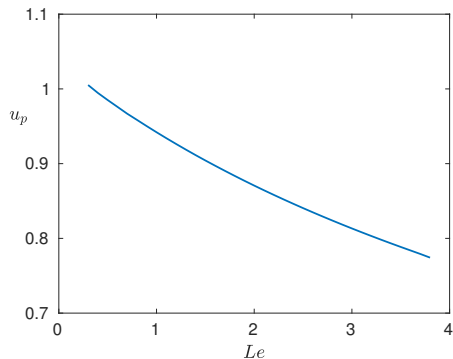


Fig. 2. Numerical values of factor  $u_p = S_d/U_L$  appearing in Eq. (6) plotted as a function of the Lewis number for  $\beta = 10$  and  $\gamma = 0.7$ . These values were kept in the present study.

Figure :  $u_p$  vs  $Le$

## Premixed flame in flat channel



$$\left\{ \begin{array}{l} \frac{\partial \theta}{\partial t} + \text{Pe} [u_f(t) + 6m y (1 - y)] \frac{\partial \theta}{\partial x} = \Delta \theta + \text{Pe}^2 \omega \\ \frac{\partial Y}{\partial t} + \text{Pe} [u_f(t) + 6m y (1 - y)] \frac{\partial Y}{\partial x} = \frac{1}{\text{Le}} \Delta Y - \text{Pe}^2 \omega \end{array} \right.$$

$$\begin{array}{l} x \rightarrow -\infty, \quad \theta = Y - 1 = 0, \quad x \rightarrow \infty, \quad \frac{\partial \theta}{\partial x} = \frac{\partial Y}{\partial x} = 0 \\ y = 0, \quad \frac{\partial \theta}{\partial y} = \frac{\partial Y}{\partial y} = 0, \quad y = 1, \quad \frac{\partial \theta}{\partial y} = \frac{\partial Y}{\partial y} = 0 \end{array}$$

# Multiplicity of steady states: $Le = 0.7$ , $m = 2$

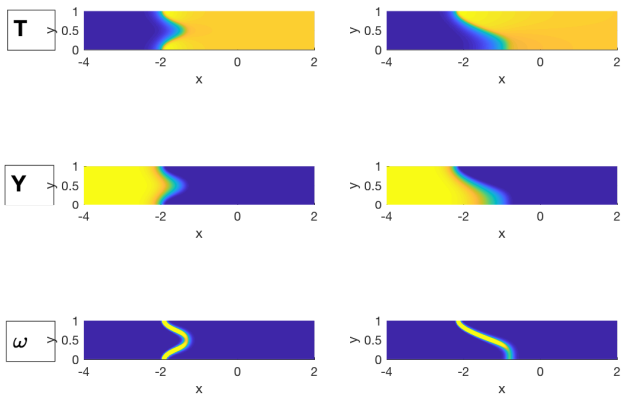


Figure : Symmetric (left) and non-symmetric (right) steady states.

Flat channel,  $u_f$  vs  $m$ 

Fig 2 V. N. Kurdyumov, Combustion and Flame, 158 (2011)

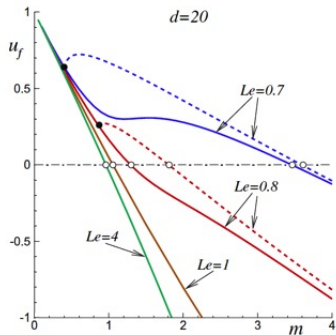
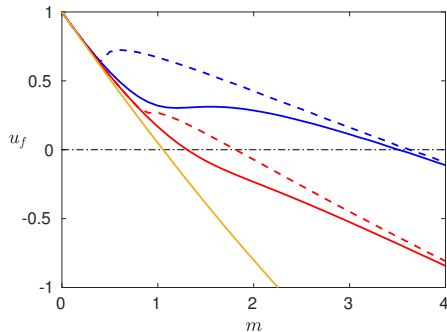


Fig. 3. Computed flame velocity  $u_f = U_f/S_L$  as a function of the non-dimensional flow rate  $m = U_0/S_L$  for several values of  $Le$  and  $d = 20$ ; solid lines – symmetric flames; dashed lines – non-symmetric flames; the symbol • marks – the bifurcation points; the symbol o – the critical flashback points.

Figure :  $u_f$  vs  $m$

# Convergence

Convergence vs.  $h$  using polynomials of degree 2, 4, 6.

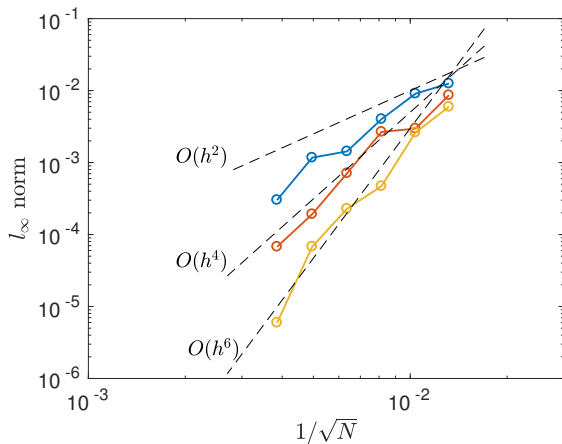


Figure : Convergence for  $Le = 1$ , compares against a solution obtained with  $N = 310,209$ .

- 1 Introduction
- 2 Mathematical model
- 3 Numerical implementation
- 4 Validation and convergence
- 5 Numerical experiments**
- 6 Conclusions

## Parameters

Table :

|       |       |                   |       |       |      |          |          |            |               |
|-------|-------|-------------------|-------|-------|------|----------|----------|------------|---------------|
| $h_m$ | $h$   | $\Delta t$        | $L_0$ | $L_f$ | $a$  | $b$      | $x_{ig}$ | $y_{ig}$   | $\delta$      |
| 0.05  | 0.025 | $2 \cdot 10^{-6}$ | -6    | 10    | 0.75 | 3        | -1.25    | 0.2        | 0.15          |
| $V$   | $m$   | $Pe$              | $Pr$  | $Le$  | $Ze$ | $\gamma$ | $\kappa$ | $\theta_m$ | $\theta_{ig}$ |
| 2     | 2     | 10                | 0.7   | 1     | 7    | 0.7      | -100     | 0          | 1             |



Isothermal,  $V = 2$ ,  $m = 2$ ,  $x_{ig} = -1.25$ ,  $y_{ig} = 0.2$

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Isothermal vs Adiabatic,  $V = 2$ ,  $m = 2$ ,  $x_{ig} = -1.25$ ,  $y_{ig} = 0.2$

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Isothermal,  $V = 2$ ,  $m = 2$ ,  $y_{ig} = 0.2$

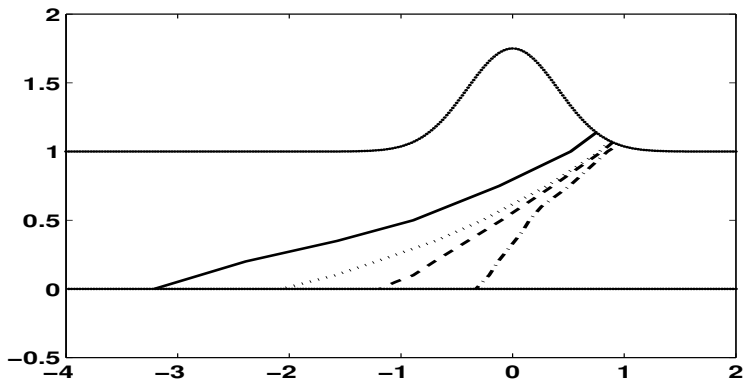
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$$x_{ig} = -1.25$$

$$x_{ig} = -1.0$$

## Hot spot location for anchored flame



**Figure :** Each line separates locations of the hot spot for which the flame gets anchored (to the left) from locations in which it is blown up. Solid line:  $m = 4, V = 0$ . Dotted line:  $m = 2, V = 2$ . Dashed line:  $m = 2, V = 0$ . Dot-dashed line:  $m = 2, V = -2$ .

- 1 Introduction
- 2 Mathematical model
- 3 Numerical implementation
- 4 Validation and convergence
- 5 Numerical experiments
- 6 Conclusions**

# Conclusions

- Simplified model of time dependent combustion in microcombustor
- Model has been validated by computing flame velocity in a channel
- Polyharmonic splines with polynomial augmentation of  $m$ -th degree results in  $O(h^m)$  convergence for steady solution
- Semi-implicit CN-AB2 for time integration
- Model yields information regarding
  - attachment of flame
  - location of hot spot for successful ignition
  - length of flame
  - fuel leakage
  - inner or outer notch, ...